

## Carbon Dioxide Fixing-Type Hydrogen Reduction Leaching of Deep-Sea Oxide Minerals Using a Pt/PTFE Catalyst in Ammonium Carbonate Solution at Moderate Temperature and Atmospheric Pressure

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### ABSTRACT

H<sub>2</sub> reduction leaching of cobalt crust was carried out to study the optimum mixing conditions of NH<sub>3</sub>-(NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>-CuSO<sub>4</sub> solutions. Cobalt and Ni was extracted 90% or higher in the 2M NH<sub>3</sub>-0.5M(NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>-0.1MCuSO<sub>4</sub> solution using a Pt catalyst loaded on polytetra-fluoroethylene (PTFE) under 60°C, 0.5atm of H<sub>2</sub> pressure, 3.3g/l of slurry concentration for 2-3h.

KEY WORDS: cobalt crust, H<sub>2</sub> reduction, hydrophobicity, ammonical leaching, Pt/PTFE catalyst

### INTRODUCTION

The deep-sea oxide minerals such as manganese nodules and cobalt crusts are expected as unlimited resources of Co, Ni and Cu in the 21st C, although their contents are low. Though many researches have been carried out including several pilot tests (Okabe and Okuwaki, 1979 a,b), it is believed that a long lead time would be required for operating the commercial plant. During the long period, it may be possible that the boundary conditions for processing are altered by the global warming due to the CO<sub>2</sub> emission. Although CO (Agarwal et al., 1978) and SO<sub>2</sub> (Rokukawa, 1992) reduction processes in NH<sub>3</sub>-(NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub> solution have been developed, one of the most promised processes under such environment is H<sub>2</sub> reduction leaching in NH<sub>3</sub>-(NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub> solutions which has not been studied yet. In such process clean H<sub>2</sub> is used as a reducing agent, and CO<sub>2</sub> emitted in the process can be fixed simultaneously as MnCO<sub>3</sub>. The problems in H<sub>2</sub> reduction leaching are poor solubility and activity of H<sub>2</sub> at low temperature. On the other hand when H<sub>2</sub> reduction is carried out at high temperature and pressure, each ion of Co, Ni, Cu in the leaching solution might be reduced to the metals. A hydrophobic Pt catalyst loaded on polytetrafluoroethylene (PTFE) membrane filters to activate H<sub>2</sub> gas and a redox couple of Cu(II)-Cu(I) ions are able to

proceed the H<sub>2</sub> reduction leaching under moderate temperature and atmospheric pressure. In the present paper, we report the optimum conditions for a H<sub>2</sub> reduction leaching of cobalt crust using a Pt/PTFE catalyst in NH<sub>3</sub>-(NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>-CuSO<sub>4</sub> solutions.

### EXPERIMENTAL

**Ore:** A cobalt crust sample(AD04) was dredged in north sea area of Samoa of Pacific Ocean. The composition is shown in Table 1. The sample was ground below 200 mesh, washed with water, and dried at 105°C for 2h.

Table 1 Chemical composition of cobalt crust ADO4/ wt%

Cu	Ni	Co	Mn	Fe
0.22	0.47	0.52	20.63	13.21

**Preparation of Pt/PTFE catalyst:** A PTFE membrane filter paper, 47 mm in diameter, pore size of 0.2 μm and 0.06 mm in thickness was cut off 8 parts equally, and then cleaned in ultrasonic bath and impregnated for 24h in a 2wt% H<sub>2</sub>PtCl<sub>6</sub>·6H<sub>2</sub>O acetone solution. After air-drying the Pt/PTFE catalyst was prepared by H<sub>2</sub> reduction at 200-250 °C for 1-2h. The amount of Pt loaded was about 12wt %.

**Leaching:** A 300ml of 2M NH<sub>3</sub>-0.5M (NH<sub>4</sub>)<sub>2</sub>CO<sub>3</sub>-0.1M CuSO<sub>4</sub> solution was poured in a 500ml 3necked-round bottom flask involving 0.5g of cobalt crusts and Pt/PTFE dipped in a water bath, and a mixed gas of H<sub>2</sub>(50%) and N<sub>2</sub> was supplied through a ball-filter after N<sub>2</sub> replacement of the air. Agitation was carried out with a magnetic stirrer. A small portion of the slurry was extracted at certain time interval and filtered. Cobalt and Ni in the filtrate were determined by ICP-AES.

### RESULTS AND DISCUSSION

**1. Effect of preparation conditions on the activity of Pt/PTFE catalyst**  
Leaching curves of Co and Ni with Pt/PTFE catalysts prepared under